Final Report on

Quenching of Solid Propellant Combustion

Grant AF-AFOSR-C897-67

March 1970

Department of Chemical Engineering



## Engineering Research

College of Physical and Engineering Sciences

Brigham Young University

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Technical supervisor for this program is Lt. Col. R. W. Haffner, project scientist, Propulsion Division, Directorate of Engineering Sciences, Air Force Office of Scientific Research.

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## SUMMARY

This final report describes the progress made in the study of propellant extention under Grant AF-AFOSR-0897-67 between March 1967 and February 1969.

At the inception of the grant period, a theory had been developed to describe solid propellant flame quenching by rapid depressurization. Comparison between theory and experiment seemed promising, and it was necessary to determine the magnitude of certain combustion parameters. An experimental technique was devised and used to determine the critical combustion parameters. The use of these parameters then revealed a discrepancy between theoretical predictions and experimental results. In fact, the discrepancy was so great as to show the theoretical model to be invalid.

Accordingly, an improved theoretical model was developed and compared to experiment. The improved theory agreed well with experiment and also explained the causes behind some previously puzzling experimental results.

## I. INTRODUCTION

This report describes research which is part of a continuing program intended to characterize propellant combustion during rapid depressurization. The research was initiated under Grant AF-AFOSR-897-65 and continued under Grant AF-AFOSR-897-67.

During the period of Grant AF-AFOSR-897-65, a simple propellant extinction theory was developed. This theory was based on a combustion model that assumed:

- 1. the heat conduction is one-dimensional
- 2. there are no reactions beneath the propellant surface
- 3. the thermal properties of the propellant are constant
- 4. the propellant is homogenous and semi-infinite
- 5. the heat transfer to the solid propellant surface was the same as the steady state heat transfer at the same pressure
- 6. the surface temperature was constant

With these assumptions, it was possible to numerically solve the heat transfer equations and describe the propellant extinction in terms of only two parameters. A dimensionless heat of decomposition and characteristic depressurization time.

Experimental extinction data were gathered to augment the data available in the literature and then these data were compared to the theory by the use of assumed heats of vaporization. The comparison was favorable in most cases but depended heavily on the value chosen for the heat of decomposition.

A simple method of doubtful reliability was used to experimentally determine the heats of decomposition for the propellants tested in this program.

Subsequent use of these values to make theoretical predictions proved discouraging, and it was at this point that the previous grant expired.

It was then necessary to find a better method for determining the propellant heat of decomposition. This was accomplished and is discussed in the next section of the paper. Use of the determined heat of vaporization showed that the theory was inadequate and hence improved extinguishment theory was derived. This theory, based on the Dennison and Baum combustion model (1), is described in section IV. As is shown in section V, the improved model agrees well with experimental observations.

## II. RADIATION AUGMENTED BURNING RATE STUDIES

Since the exact value for the propellant heat of decomposition was so critical in comparing experiment and theory, it seemed desirable that the parameter be determined by a more reliable procedure. Accordingly, an experiment was devised to yield data from which the burning propellant surface temperature and heat of decomposition could be calculated.

The technique involved first determining the burning rate of propellant in a chamber whose wall temperature was fixed at different values in different tests. Then, the burning rate of the propellant was determined when the propellant was the shape of a long, thick-walled cylinder and the internal cylinderical surface burned. It was then reasoned that a simple strand of propellant burning in a chamber with cold walls experienced a net radiative heat loss and the burning rate would be smaller because of the heat loss. However, as the chamber wall temperature was raised, the point would be reached where there were no radiative heat losses and the combustion would be adiabatic. This would be exactly analogous to combustion inside a long hollow cylinder where the radiative losses would be negligible. The propellant surface temperature could be calculated from the chamber wall temperature that caused the propellant to burn at the same rate as did the internally burning cylinder. For the PBAN-AP propellant tested, Fig. 1 shows the surface temperature to be 560°C in excellent agreement with the experimental data of others (2,3).

It was found that the burning rate of the propellant increased linearly as the flux from the chamber wall to propellant surface increased. A computational scheme was developed that permitted us to calculate the heat of decomposition for the burning propellant. The scheme is outlined as follows:

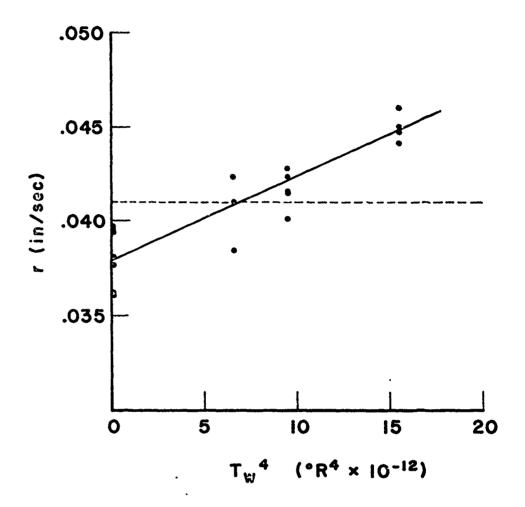


FIGURE 1 - Strand-burning rates as a function of wall surface temperature.

The dotted line corresponds to the burning rate of an internal-burning cylinder.

1. The propellant burning rate  $(\overline{r})$  is assumed to be a function of flame temperature  $(T_f)$  and radiant flux level  $(f_r)$  as

$$r = f(f_r, T_f)$$

2. The derivative of this equation is found to be

$$\frac{d\overline{r}}{df_{r}} = \frac{\partial \overline{r}}{\partial f_{r}} + \left(\frac{\partial \overline{r}}{\partial T_{f}}\right) \frac{dT_{f}}{df_{r}}$$

- 3. A heat balance is made at the interface; the gaseous products are assumed to have a characteristic reaction time and then the partial derivatives are written in terms of the unknown heat of decomposition  $(\gamma)$  and several parameters whose values are known.
- 4.  $\frac{dT_f}{df_r}$  is evaluated from an overall heat balance.
- 5. The above results are combined, small order terms neglected and the resultant equation is

$$\frac{d\overline{r}}{df_{r}} = \frac{1}{2\rho_{s}[Cs(T_{s} - T_{o}) + L]} \left[ 1 + \frac{C_{s}(T_{s} - T_{o}) + L}{C_{g}(T_{fo} - T_{s})} \right]$$

when  $\rho_S$  is the propellant density,  $C_S$  is its heat capacity,  $C_g$  the mean heat capacity of the gases and  $T_S$ ,  $T_O$ , and  $T_{fO}$  are respectively the surface temperature, the conditioning temperature, and the adiabatic flame temperature.

6. The value for the heat of decomposition, L, is found by rearranging the equation and using known values for the parameters except  $d\overline{r}/df_r$ , which is the slope of the heat flux-burning rate curve and is evaluated from Fig. 1.

For the propellant tested, the heat of decomposition was found to be -130 cal/g in excellent agreement with previous work (2). This number means that there is an exothermic reaction at or near the propellant surface.

The fact that the decomposition process was exothermic proved to be very significant. Previously, the decomposition was assumed to be endothermic and all calculations were made on that basis. When the correct exothermic value was used in the theory and the theoretical predictions examined, they were found to be totally unrealistic. In fact, it was found that a decrease in pressure was predicted to cause an increase in burning rate. A relation totally at variance with the known facts.

## III. EXTINCTION AND OTHER COMBUSTION CHARACTERISTICS:

A readily extinguishable propellant is one whose burning rate is easily made to approach zero by a given pressure transient. Mathematically, the value of  $\frac{dr/r}{dp}$  is large for such a propellant. Similarly, a propellant very susceptible to oscillatory combustion has a large value for the real part of the response function  $\frac{dr/r}{dp/p}$ . The similarity of the two groups suggests that a very extinguishable propellant may also be one very prone to oscillatory combustion.

This potential relationship was investigated by determining the extinction characteristics of several propellants whose oscillatory combustion was studied elsewhere (4,5). Specifically, a mesa-type base (X-14) a conventional double base (JPN) a polyurethane (JPL 534), and a polysulphide (T-35), were tested. Each of these propellants has been used in a developmental motor and each has exhibited severe oscillatory combination.

The experimental results are shown in Table 1 and clearly indicate that there is no simple relation between extinguishability and instability. In fact, the two double-base propellants are about equally unstable but differ in ease of extinguishability by two orders of magnitude.

Propellant	$ \begin{pmatrix} \frac{\mathrm{d}\mathbf{r}/\mathbf{r}}{\mathrm{d}\mathbf{p}/\mathbf{p}} \end{pmatrix}_{\mathrm{Re}} $	Critical denp
JPN	2.6	- 7
X-14	2.4	- 700
JPL 534	1.2	- 20
T-35	1.4	- 80

It was pointed out previously (9) that there is a correlation between extinguishability and the burning rate near the deflagration limit. However, the burning rate near the deflagration limit is a parameter rarely measured and reported. Therefore, during this period little additional data have been found. Such data as were found supported the correlation but it is concluded that at this time the use of such a seldom-measured parameter has limited utility.

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## IV. THEORY

## 1. Review of Previous Models

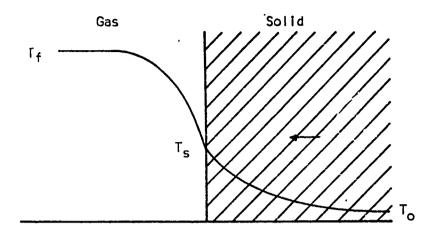
Mathematical models of the process of rapid depressurization extinguishment of a burning solid propellant have been proposed by at least a dozen different authors. According to a recent paper by Merkle, et. al. (6), the universal approach has been to assume that the extinguishment process occurs because of a deficiency in the heat flow from the flame to the burning surface and into the unburned solid, this heat flow being a function of the pressure. This statement applies to the present approach.

To describe the heat flow, the solid propellant is considered to be represented as a semi-infinite slab in order that only one-dimensional heat transfer need be considered. Figure (2) shows the geometrical model of the process along with the general shape of the temperature profile, which extends from the completely reacted products of combustion at the adiabatic flame temperature,  $T_f$ , to the initial conditioning temperature of the propellant,  $T_0$ . For further simplification, the burning surface is taken as the reference point for the position coordinate x, the propellant assumed to move to the left at its burning rate in order to maintain the burning surface at a fixed position.

An energy balance taken on an element of the solid of thickness dx results in the following partial differential equation:

$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2} + r \frac{\partial T}{\partial x}$$
 (1)

where  $\alpha$  is the effective thermal diffusivity of the solid and r is the burning rate. This equation is easily integrated for the steady-state ( $\partial T/\partial t = 0$ ) to yield the following equation for the temperature profile in the solid:



Geometrical Model of Burning Propellant

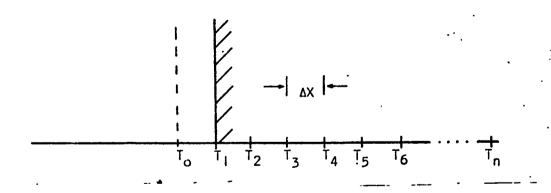


FIGURE 2 - Method of Separating Solid into Finite Difference Elements

$$T = T_o + (T_S - T_o) \exp(-\overline{r} \times / \alpha)$$
 (2)

where  $T_S$  is the temperature of the burning surface and  $\overline{r}$  is the steady-state burning rate. The heat flux that must be supplied to the solid to maintain this profile, in addition to that necessary to gasify or decompose the solid, is given by

$$f_{S} = \rho c_{S} \overline{r} (T_{S} - T_{O})$$
 (3)

and the thermal energy stored in the solid above its initial conditioning state is

$$q_s = (k / \overline{r}) (T_s - T_0)$$
 (4)

where k is the thermal conductivity.

The original models of Von Elbe (7) and Paul (8) were the first to consider the non-steady-state heat flow problem with the objective of predicting extinguishment conditions. These models are very similar and do provide insight into the physical processes that might lead to extinguishment even though they are based on rather gross simplifying assumptions. The Paul model is outlined here to provide a historical reference for comparison with the model developed for this study.

Paul assumed that as a first approximation the surface temperature remained constant. He further took the steady-state burning rate to be related to the pressure by

$$\overline{r} = a p^n$$
 (5)

and assumed that the flux into the solid during either steady-state or transient periods could be expressed as

$$f_s = \rho c_s \overline{r} (T_s - T_o)$$
 (6)

For a transient case,  $\bar{r}$  would be interpreted as the steady-state rate corresponding to the instantaneous value of the pressure. During a transient period, the energy stored in the solid must change as the burning rate changes. Both Von Elbe and Paul assumed as a first approximation that this stored energy adjusts instantaneously with changes in burning rate, its magnitude always being given by Equation 4. Thus, during a transient period, the required flux is

$$f_s = \rho c_s r (T_s - T_o) + dq_s / dt$$
 (7)

Combining (4) and (5) and carrying out the differentiation yields

$$dq_{s}/dt = -\frac{nk}{r} (T_{s} - T_{o}) \frac{d\ln p}{dt}$$
 (8)

and combining (6), (7), and (8) yields

$$r = \overline{r} \left[1 + (n\alpha/\overline{r^2}) \frac{d \ln p}{dt}\right]$$
 (9)

Equation 9 predicts that the instantaneous rate will drop to zero whenever

$$\left(\frac{\mathrm{dln}\ p}{\mathrm{dt}}\right)_{\mathrm{Ext.}} = -\overline{r}/n\alpha \tag{10}$$

Since it was observed that this equation only qualitatively correlated experimental extinguishment data, a correction factor,  $\lambda$ , was added to bring it into quantitative agreement, or

$$\left(\frac{\mathrm{dln} \ p}{\mathrm{dt}}\right)_{\mathrm{Ext.}} = -\lambda \overline{\mathbf{r}}/\mathrm{n}\alpha$$
 (11)

Horton (9) recognized that a serious shortcoming of the Paul and Von Elbe theories was the assumption that the heat stored in the solid adjusted instantaneously to changes in burning rate. In reality when a change in pressure and corresponding heat flux to the solid occurs there is a time lag before a new steady-state profile is established. To treat the transient conduction process more exactly, Horton carried out a numerical integration of the non-steady-state differential energy balance equation (Equation 1). He further improved the theory by including the energy required for gasification of the solid in the solid heat flux equation. His equation, corresponding to Equation 6, for the flux supplied to the solid is

$$f_{s} = \overline{r} \rho \left[ L + C_{s} (T_{s} - T_{o}) \right] - r \rho L$$
 (12)

where L is the effective heat of gasification of the solid. The flux required by the solid in Horton's model, corresponding to Equation 7, is obtained from the numerical integration of the differential energy balance. As in the Paul model, the criterion for extinguishment is that the rate becomes zero as a consequence of the supplied  $f_s$  being entirely absorbed by the solid in changing  $q_s$ , the amount of heat stored.

Horton's model predicts for an exponential pressure decay and for a given  $T_{\mbox{\scriptsize f}}$  and  $T_{\mbox{\scriptsize s}}$  that

$$\left(\frac{d \ln p}{dt}\right)_{Ext.} = -\lambda_{H}(\overline{r}^{2}/\alpha)$$
 (13)

where  $\lambda_{\rm H}$  is a function of n, L<sub>s</sub>, and P<sub>a</sub>/P<sub>o</sub>, the latter being the ratio of the final pressure following depressurization to the initial pressure. The function  $\lambda_{\rm H}$  is described in terms of graphs developed from the results of the numerical calculations.

Comparing (13) with (11) shows that  $\lambda_H$  corresponds to the correction factor  $\lambda$  employed with the Paul theory. Thus, Horton's theory provides a method of evaluating  $\lambda$  in terms of more fundamental parameters.

During the course of the present contract, it was discovered that Horton's model yielded erroneous results if the heat of gasification, L, were negative. This was considered to be a serious shortcoming since, as discussed in Section II, there is evidence suggesting this parameter can indeed be negative for some propellants.

More recent models have been proposed by Wooldridge (10) and by

Summerfield (11). The latter model is based upon the Granular Diffusion Flame

Theory of Summerfield, which does not provide the proper dependence of steadystate burning rate on pressure for many propellants. Wooldridge's approach was

to modify a combustion theory originally proposed by Denison and Baum (1).

This same approach has been followed in the present study. The unique feature

of the present approach is that the Denison-Bair theory is used only to predict

deviations from the steady-state conditions; the conventional steady-state

strand-burner data is employed as fundamental input data.

## 2. Development of Present Model

The Denison-Baum model was originally derived as a simplified transient combustion model for application to combustion instability problems. Rather than employing a constant burning surface temperature, as Horton did, this model uses an Arrhenius-type relationship between burning rate and temperature.

$$r = A \exp \left(-E_{s}/RT_{s}\right) \tag{14}$$

It is further assumed that the rate is coupled to the flame temperature,  $\mathbf{T}_{\mathbf{f}}$ , and pressure by the following equation

$$r = BP^{N} T_{f}^{N+1} \exp (E_{f}/RT_{f})$$
 (15)

In the present analysis these equations have been replaced with

$$r = \overline{r}_{p} \exp \left[ \left( -E_{s}/R \right) \left( 1/T_{s} - 1/\overline{T}_{s}, p \right) \right]$$
 (16)

and

$$r = \overline{r}_p (T_f / \overline{T}_f)^{n+1} \exp [(-E_f / R) (1 / T_f - 1 / \overline{T}_f, p)]$$
 (17)

where  $\overline{r}_p$ ,  $\overline{T}_{s'p}$ , and  $\overline{T}_{f'p}$  are the steady-state burning-rate, surface temperature, and flame temperature at the instantaneous pressure p, and n is the empirical value of  $d\ln \overline{r}_n/d\ln p$ .

The most important feature of the Denison-Baum theory is the equation for the rate of heat conduction into the solid beneath the burning surface. This equation may be written as

$$k \frac{\partial T}{\partial x} x = 0 + = -r \rho_s [C_s (T_s - T_\infty) + C_g (\overline{T}_f - T_f)]$$
 (18)

with the origin of the x coordinate fixed on the burning surface, the positive direction extending into the solid. This equation is obtained by combining overall energy balances for both steady and non-steady conditions, eliminating energy terms associated with the surface gasification reaction. The virtue of this equation is that data for surface and flame temperatures are more readily available than data for effective heats of gasification. Calculation of the numerical value of the instantaneous heat-flux supplied to the solid is also straight-forward. Given instantaneous values of  $T_{\rm S}$  and  $P_{\rm S}$  r is computed from (16) and  $T_{\rm f}$  is computed from (17). These values then given the instantaneous value of the flux to the solid when substituted into (18).

The most difficult problem in employing either the Horton or the Denison-Baum models in predicting extinguishment conditions is the calculation of the rate of transient heat conduction into the solid propellant. The usual numerical technique for solving the differential energy balance which describes the transient heat transfer process, Equation (1), is to separate the solid into finite difference elements such that the energy balance on each element can be written as an algebraic equation rather than a differential equation. The algebraic equations, one for each of the finite elements, are then solved simultaneously to obtain both the temperature profile at any given instant during the transient period and the increment of change at any position for a given increment in time.

Since sophisticated numerical techniques have become available for the simultaneous solution of a set of ordinary differential equations, two recent authors (12, 13) have pointed out the advantage of using these techniques to solve transient heat conduction problems. The differential energy balance for both finite elements is transformed into an ordinary differential equation applying finite difference methods to the space derivatives only. Available differential equation-solving programs are then employed to carry out simultaneous integration of these equations to compute the variation of the temperature profile with time. This approach has been adopted in this study.

Figure 2 illustrates the method of separating the solid into finite elements. The ordinary differential equation which approximates the energy balance for each element is written as

$$\frac{dTi}{dt} = \alpha \left[ \frac{T_{i-1} - 2T_i + T_{i+1}}{(\Delta X)^2} \right] + r \left[ \frac{T_{i+1} - T_{i-1}}{2\Delta X} \right]$$
(19)

The wide variation of r during the extinguishment transient presents special problems in the numerical solution of the transient conduction equation. This problem is illustrated by considering the change in the depth of penetration of the temperature profile during the transition from one steady-state condition to another, the first condition being that prior to depressurization and the other the condition after a depressurization has occurred, the propellant assumed to continue burning. The steady-state temperature-profile is described by

$$\frac{\overline{T} - T_{\infty}}{T_{S} - T_{\infty}} = \exp(-\overline{r}x/\alpha)$$
 (20)

Suppose that during the transient the rate is reduced by a factor of 10. Equation (21) shows that the depth at which a given temperature is established in the solid is then increased by a factor of 10. Suppose further that 20 equal elements of width  $\Delta X$  are selected at the start, the final element chosen such that its temperature rise was only 5% of the rise at the surface. The temperature rise of this element when the new steady-state is established would be 74% of the surface rise; 200 elements of width  $\Delta X$  would now be required to reach a depth where the rise was only 5%. Since a separate equation must be solved for each element, the problem can become unwieldy if equal-sized elements are employed and the burning rate change is large.

Marxman and Wooldridge (10) suggests that the problem of excessive finite elements can be circumvented by employing the transformation

$$1 - Y = \exp(-rx/\alpha) \tag{21}$$

to define a new distance variable Y. This variable ranges from 0 to 1 as X ranges from 0 to  $\infty$ , and elements of equal width  $\Delta Y$  correspond to  $\Delta X$  elements

which become successively wider as X increases, the last element having the width . This transformation has been investigated during this study and found to lead to erroneous results if the rate varies widely. A different transformation has been found to better accomplish the desired reduction in finite elements and also retain the accuracy of the numerical integration method. In this transformation the new distance variable, y, is defined by

$$\frac{\mathrm{d}y}{\mathrm{d}x} = \frac{\mathbf{r}}{\alpha} (1 - \mathbf{y}) \tag{22}$$

The corresponding finite element spacing is

$$\Delta x = (\alpha/r) \Delta y/(1 - y) \tag{23}$$

Letting y range between zero and one and taking  $\Delta y$  as a fixed quantity, the finite difference spacing,  $\Delta x$ , increases regularly with both increasing depth beneath the surface and decreasing burning rates. The resulting finite difference equation in non-dimensional form that was used in place of Equation (1) is

$$\frac{d\theta_{i}}{d\tau_{s}} = a_{i}R^{2}(\theta_{i-i} - \theta_{i} + \theta_{i+1}) - b_{i}c_{i}(\theta_{i+1} - \theta_{i-1}) \quad (1/R) \quad \frac{dR}{dT_{s}}$$
 (24)

with

$$\theta_i = T_i/T_o$$

$$\tau_s = \overline{r}^2 t/\alpha$$

$$R + r/\overline{r}$$

$$a_{i} = (1 - y)(1 - y_{i} - \Delta y / (\Delta y)^{2}$$
 (25)

$$b_{i} = \int_{j=0}^{i} \Delta y/(1 - y_{i})$$

$$c_i = (1 - y_i)(1 - y_i - \Delta y)/(2 - 2y_i + \Delta y)$$

The last term on the right-hand side of Equation (25) accounts for adjustment of the temperature as the mid-point of the finite element is shifted along the x axis due to changes in r. This term does not appear in the equation for the surface temperature (which becomes  $T_1$ ) since this point is stationary.

The surface boundary condition, Equation (18), was expressed in finite-difference form by defining a station at a position y above the surface with a fictitious temperature  $T_{\rm o}$ :

$$T_{o} \equiv T_{2} + 2\Delta x_{o} \left(k \frac{\partial T}{\partial x}\right)_{x=0+}$$
 (26)

where  $T_2$  is the temperature at the first station beneath the surface.

Initial calculations were made solving Equations 16, 17, 18, 24, 25, and 26 simultaneously along with the following equation describing an imposed depressurization rate.

$$\frac{dP}{d\tau_s} = - (P - P_A)(0.693/\tau_{2})$$
 (27)

A standard computer program for integrating simultaneous ordinary differential equations based on Adams method (15) was employed. The Fortran Coding for carrying out these calculations using the BYU Librascope L-3055 computer is included in the Appendix.

## V. COMPARISON BETWEEN THEORY AND EXPERIMENT

A series of parametric calculations have been made both to determine a consistent set of parameters for correlating observed extinguishment conditions and to determine the sensitivity of the model to variations in the individual parameters.

A rough correlation of existing depressurization extinguishment data is shown in Figure 3, where the time corresponding to reducing the pressure to one-half the initial value is plotted versus the initial burning rate. The data points represent limiting conditions for extinguishment to occur. If the is greater than that indicated by the data point and the initial rate is the same, the propellant will continue to burn rather than extinguish.

The line correlating this data can be represented by the equation

$$t_{k} = 0.5/\bar{r}^2$$
 (28)

where  $t_{1\over 2}$  is in milliseconds and  $\overline{r}$  is in inches per second. The rate of depressurization is assumed exponential with  $P_a/P_o$  assumed negligible compared to unity.

The non-dimensional half-time corresponding to (28) is

$$\tau_{1_{S}} = 0.5(10^{-3})/\alpha \tag{29}$$

Thus, if  $\alpha$  is again assumed to be 2.5(10<sup>-4</sup>) in.<sup>2</sup>/sec., the value of  $\tau_{\frac{1}{2}}$  corresponding to extinguishment is 2.

Figure 4 shows predicted burning rates during depressurization transients for  $\tau_{\rm L}$  = 1.5 using the following set of parameters:

Es = 30 Kcal/gm. mole

Eg = 30 Kcal/gm. mole

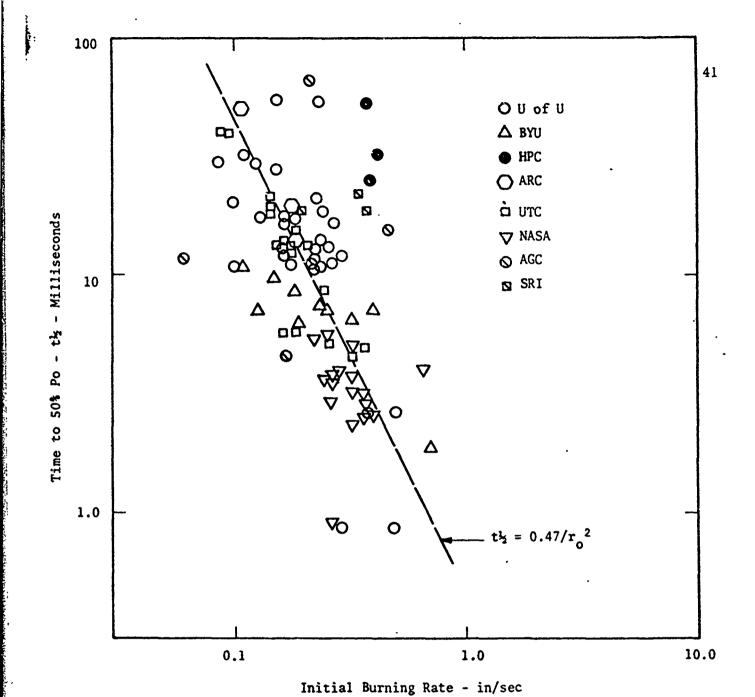


FIGURE 3 - Results of attempt to correlate marginal p extinguishment with initial burning rate

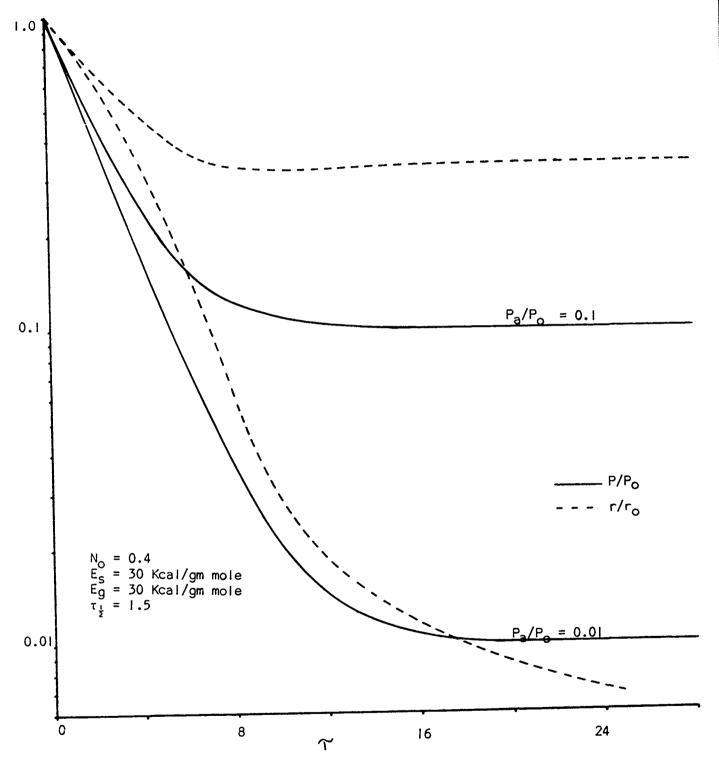


FIGURE 4 - Predicted Termination Transients for  $\tau_{\frac{1}{2}}$  = 1.5.

$$T_o = 298^{\circ}K$$
 $T_f = 10 T_o$ 
 $T_s = 3 T_o$ 
 $n = 0.4$ 
 $P_a/P_o = 0.1, 0.01$ 

 $C_g/c = 1.0$ 

The burning rate is shown to establish a new steady-state value following depressurization to  $P_a/P_o = 0.1$ ; however, it is shown to continue to decrease following depressurization to  $P_a/P_o = 0.01$ , the ratio r/F dropping far below the value corresponding to steady-state at the pressure following depressurization. This latter behavior is considered to represent the extinguishment process, the reasoning being that combustion will not be sustained below some absolute minimum rate (or absolute minimum Ts). For example, if the initial rate were 0.2 inches per second, the predicted rate for the case of  $P_a/P_o$  = 0.01 at  $\tau$  = 24 is 0.0014 inches per second. Since rates this low are not observed experimentally during steady-state conditions, it seems improbable that rates this low would exist during a transient condition. Thus it is predicted that if  $\tau_{i_2}$  = 1.5 extinguishment would become marginal at some value of  $P_a/P_o$  lying between 0.01 and 0.1 for this particular set of propellant parameters, and since  $\tau_{\frac{1}{2}}$  = 2.0 is required to correlate the experimental data, as discussed above, this particular combination of parameters yields reasonably good agreement between theory and experiment.

A series of computations has been made to determine the effect of varying the gas-phase and solid-phase global activation energies. The results of these calculations are shown in Figures 5 and 6. Increasing either  $E_s$  or  $E_g$  is shown to result in greater susceptibility to extinguishment. This effect is most strikingly shown in Figure 5 where with  $E_g$  = 15 a new steady-state burning rate is established following depressurization while with  $E_g$  = 30 the rate continues to decrease.

Figures 7, 8, 9, and 10 present the results of a series of calculations where  $P_a/P_o$  and  $\tau_{1/2}$  were systematically varied. These calculations show a rather strong dependency of the value of  $\tau_{1/2}$  required for extinguishment on  $P_a/P_o$ . Assuming that extinguishment corresponds to the case where r/r is predicted to drop below 0.05, the following table summarizes the predicted conditions for extinguishment derived from this set of calculations.

$\frac{P_a/P_o}{a}$	$(\tau_{\frac{1}{2}})$ Extinguish
0.01	10-20
0.05	1-3
0.10	0.1-0.5
0.50	< 0.01

These results suggest that the  $\tau_{\frac{1}{2}}$  required for extinguishment varies roughly with the inverse square of  $P_a/P_o$ . This information may provide some explanation for the scatter in the correlation of experimental data shown by Figure 3.

The model for the solid propellant combustion process has also been combined with equations describing the transient ballistics of a solid rocket motor. Equations expressing conservation of both mass and energy inside the motor cavity have been derived previously (14). In the present study these equations have been used in the following form:

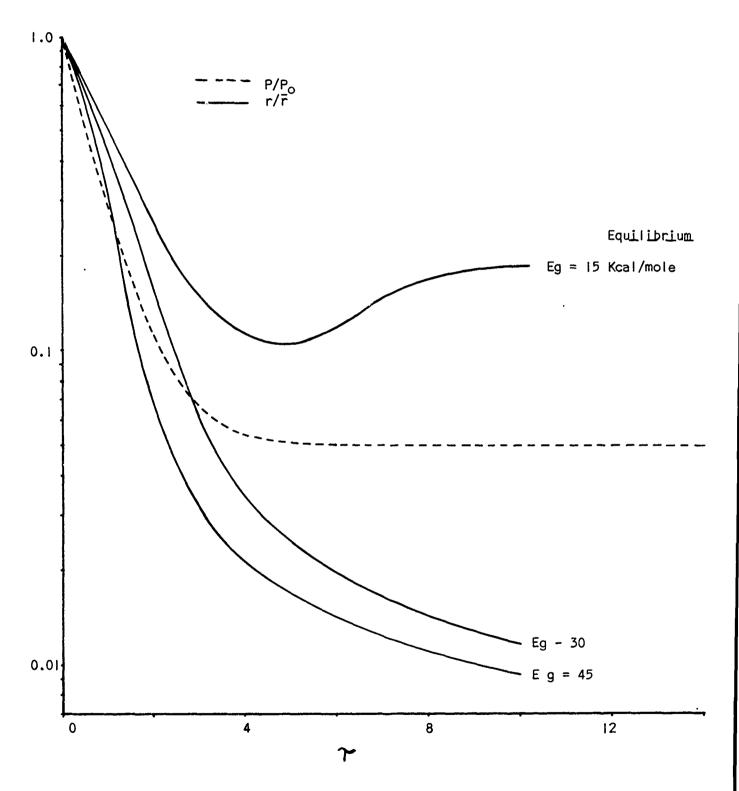


FIGURE 5 - Predicted Effect of Varying  $E_g$ 

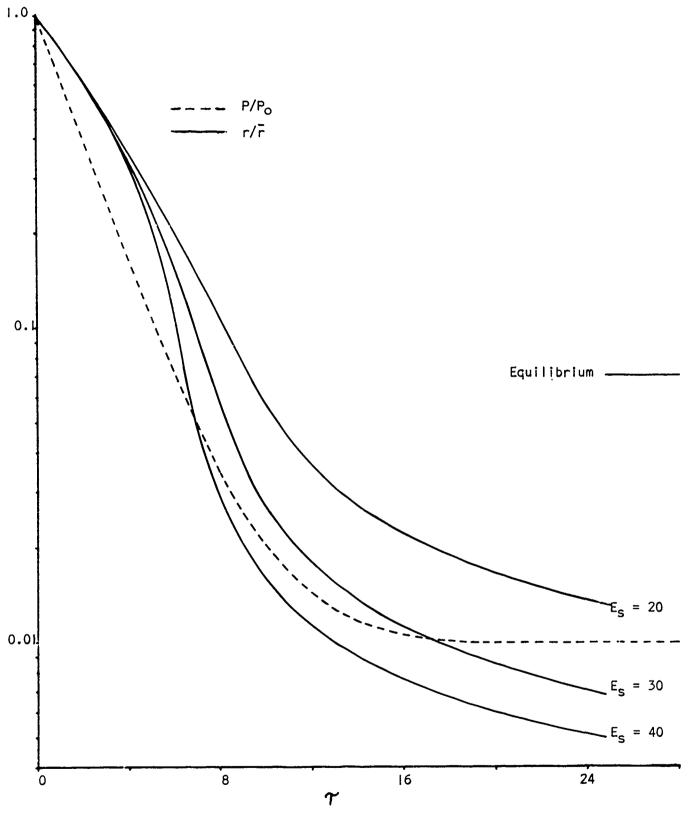


FIGURE 6 - Predicted Effect of Varying E<sub>s</sub>

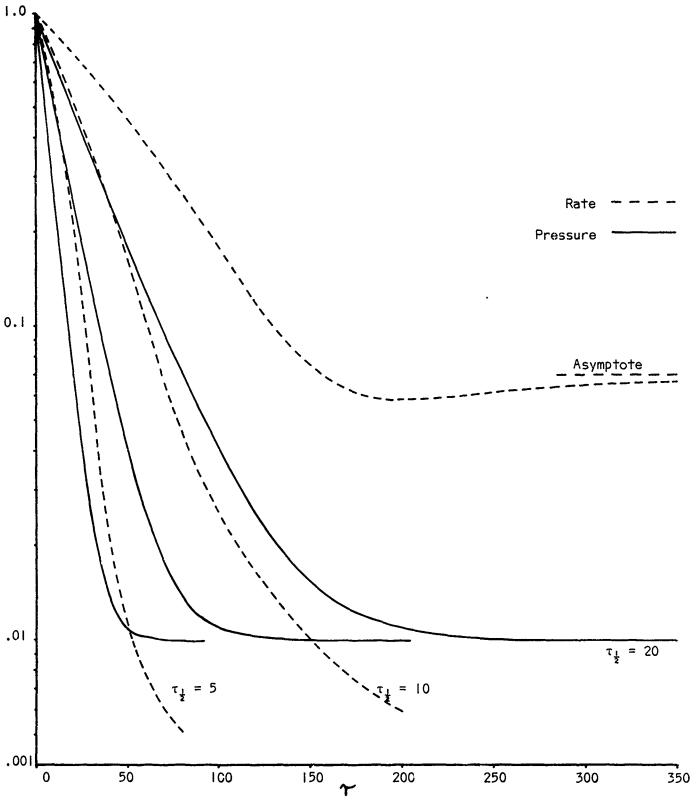


FIGURE 7 - Predicted Effect of Varying  $\tau_{\frac{1}{2}}$  for  $P_a/P_o$  = 0.01

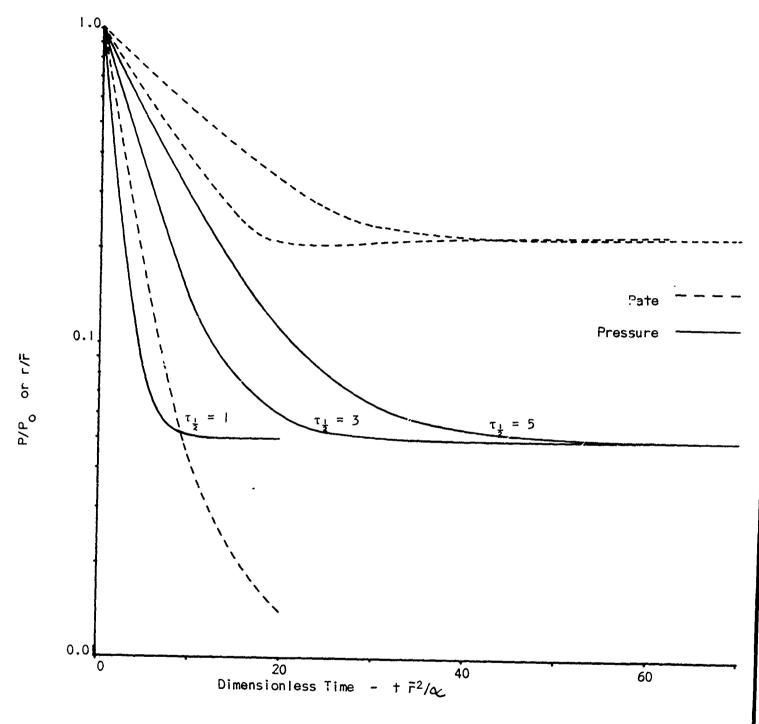


FIGURE 8 - Predicted Effect of Varying  $\tau_{\frac{1}{2}}$  for  $P_a/P_o = 0.05$ 

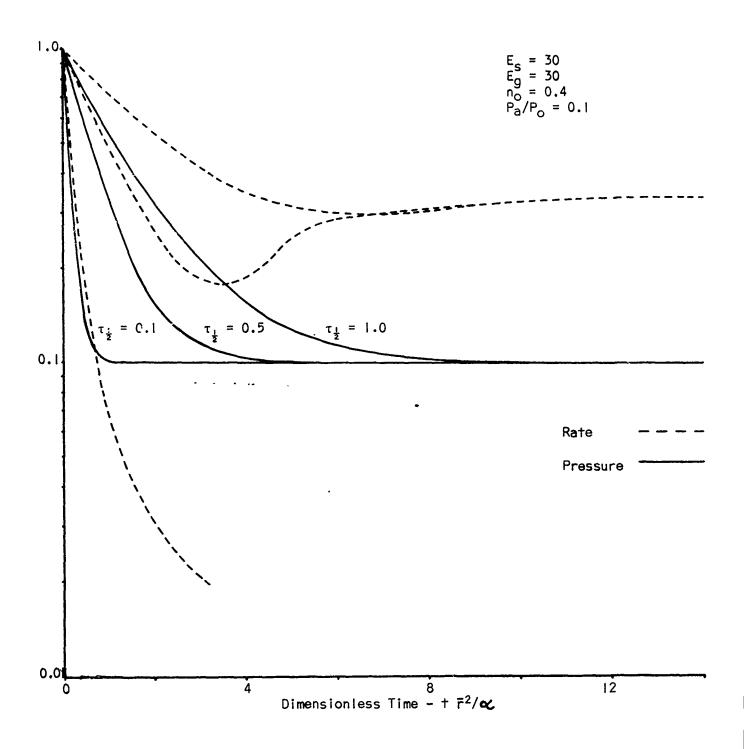
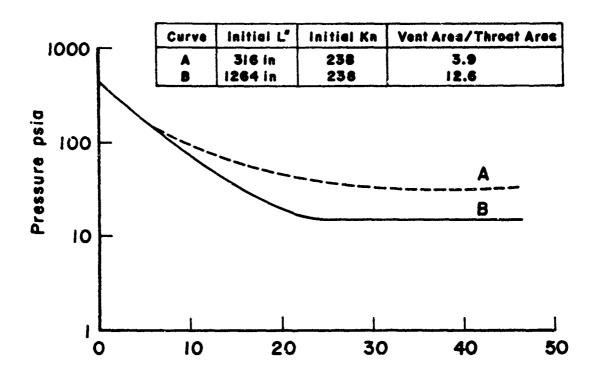


FIGURE 9 - Predicted Effect of Varying  $\tau_{\frac{1}{2}}$  for  $P_a/P_o$  = 0.1



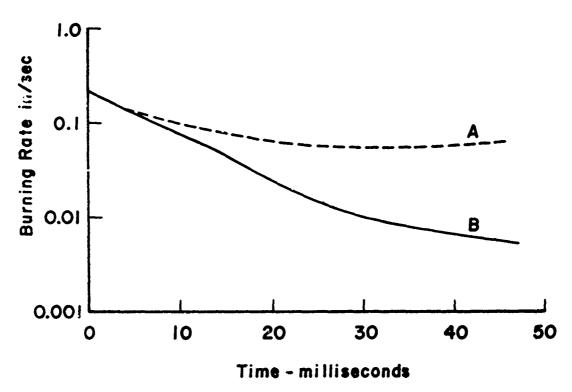


FIGURE 10 - Predicted termination transients showing the effect of varying the initial L\*, the initial  $K_n$  and dP/dt constant

$$dP/d\tau_c = \gamma R\theta_f/\overline{\theta}_c) (1 - (\theta_c/\theta_f) (R_N/R)$$
 (30)

$$d\theta_{c}/d\tau_{c} = (\theta_{c}/P)(\theta_{c}/\overline{\theta}_{c})(R)[1-\gamma+(\frac{\gamma\theta_{f}}{\theta_{c}}-1)(R/R_{N})]$$
(31)

with

$$P = p/\overline{p}$$

$$\tau_{c} = t/(L^{*}/r^{2}C^{*})$$

$$\gamma = (C_{p}/C_{v})_{gas}$$

$$\theta_{f} = T_{f}/\overline{T}_{f}$$

$$\theta_{c} = T_{c}/\overline{T}_{f}$$

$$R_{N} = (\overline{\theta}_{c}/\theta_{c})^{\frac{1}{2}PA}$$

$$A = (A_{vent} + A_{t})/A_{t}$$

Prediction of the instantaneous pressure versus time requires the simultaneous numerical integration of these equations along with those discussed earlier for the solid and the use of the steady-state burning relation. Provision has been made in the program to use the Summerfield Equation, the Vielle equation, or a table relating the burning rate to pressure. In all three cases, extinguishment is taken to occur if the rate becomes less than the burning rate at the deflagration limit of the propellant.

Tables II and III show results of calculations made with the combined combustion-ballistics model.

Table II

Predicted effect of various parameters on extinguishment of a propellant that follows the Summerfield burning rate equation

Parameter Varied	_	rinal Extinguishment  1 Depressurization Rate -(p/p) 0
Reference*	2.8-2.9	145-152
To = $100$ °C	3.6-3.7	204-211
$E_s = E_g = 25$	2.7-2.8	137-145
E = 28	2.7-2.8	137-145
$E_g = 28$	2.7-2.8	137-145
E <sub>s</sub> = 35	2.7-2.8	137-145
$E_g = 35$	2.5-2.6	125-130
T = 382	3.7-3.8	211-218
$T_{f} = 2185$ °K, L* = 364, C* = 3910	2.6-2.7	101-107
$T_{f} = 2185^{\circ}K$ , $C^* = 3910$ , $K_{n} = 274$	2.5-2.6	108-115
$Kn = 275$ , $L^* = 364$ , $Po = 667$	3.3-3.4	159-166
$Kn = 325$ , $L^* = 432$ , $Po = 886$	3.9-4.0	171-176
$Kn = 188, L^* = 250, Po = 340$	2.2-2.3	121-131
$Kn = 375$ , $L^* = 497$ , $Po = 1124$	4.5-4.6	179-184
Kn = 325, Po = 886	3.6-3.8	203-218
Kn = 375, Po = 1124	4.0-4.1	232-239
Kn = 188, Po = 340	2.4-2.5	106-114
Kn = 275, Po = 667	3.2-3.3	174-182
L* = 1000	4.0-4.1	80-83
L* = 105	2.2-2.3	254-274
$C_s/C_g = 1.0$	3.2-3.3	174-182
$Kn = 274$ , $C^* = 3910$	2.5-2.6	108-115
*The reference propellant and mo	tor had the following p	roperties:
To=25°C		sure=15 psia
$Kn=238$ $P_s=.062$ lbs/in	gropellant a	rea=8.3 in <sup>2</sup>

To=25°C	T <sub>e</sub> =600°C	ambient pressure=15 psia
Kn=238	$P_s = .062 \text{ lbs/in}^3$	propellant area=8.3 in <sup>2</sup>
L*=316 in	Y=1.22	nozzle open time=.001 sec
T <sub>f</sub> =2910°K	C*=4500 ft/sec	burning rate at 1000 psi=.33 in/sec
$C_{\rm s}/C_{\rm g}=.75$	E <sub>s</sub> =21 K cal	exponent at 1000 psi=.4
P <sub>o</sub> =520 psia	E <sub>g</sub> =21 K cal	burning rate at deflagration limit=
$r_0 = .25$ in/sec	•	.009 in/sec

Table III

Effect of various parameters on extinguishment of a propellant that follows the Vielle burning rate equation

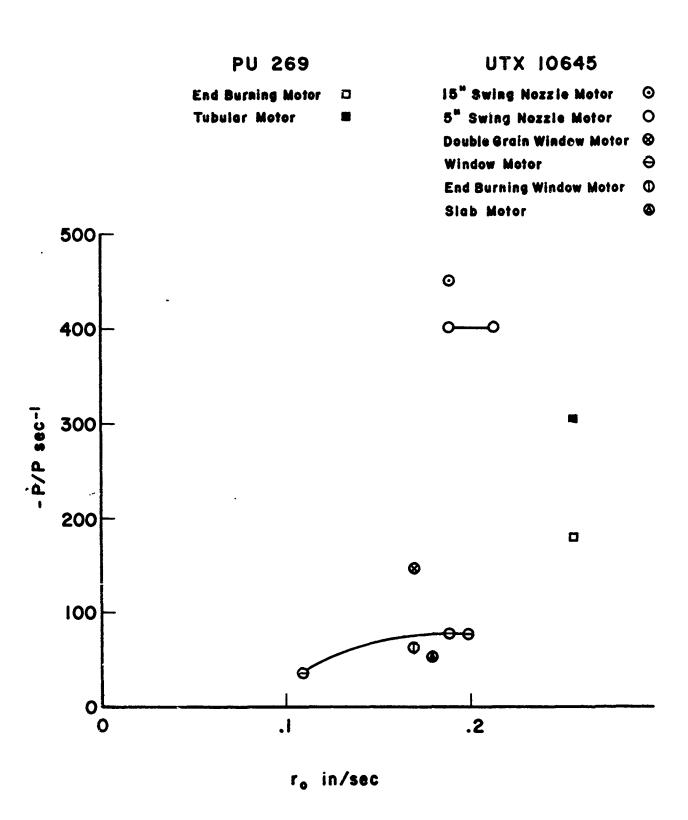
Parameters different than reference	Extinguishment A2/A1	Occurs between -(p/p)o
Reference*	3.2-3.3	177-185
n = .7	1.7-1.8	59-68
n = .3	9.0-9.25	554-569
burning rate at deflagration limit = .003	3.2-3.3	177-185
$K_n = 415$ , L* = 582 ro = .144	2.7-2.8	78-82
$K_n = 166$ , L* = 221 ro = .360	3.7-3.8	292-303
$K_{\rm n} = 1190$ , L* = 1580 ro = .0495	2.3-2.4	23-24
$K_{n}^{II} = 131$ , L* = 174 ro = .480	4.2-4.3	425-499

\*The reference propellant and motor had the following properties:

To = 25°C	$T_s = 600$ °C	ambient pressure = 15 psia
$K_{n} = 238$	$P_s = .062 lbs/in^3$	propellant area = $8.3 \text{ in}^2$
L* = 316 in	$\gamma = 1.22$	nozzle open time = .001 sec
$T_{f} = 2910^{\circ} K$	C* = 4500  ft/sec	rate at 520 psi = .25 in/sec
$C_s/C_g = .75$	$E_s = 21 \text{ K cal}$	n = .5
P = 520 psia	$E_g = 21 \text{ K cal}$	r at deflagration limit = .009
$r_0 = .25 \text{ in/sec}$	•	

One of the parameters noted to have a significant influence on marginal extinguishment conditions was the initial L\* of the motor. Additional calculations in which this parameter was varied by a factor of 4 again showed the importance of the overall pressure drop. In these calculations the initial burning area/throat area ratio and initial depressurization rate were held constant by adjusting the venting area. The results of these calculations are shown in Figure 10. Because a much larger vent area/throat area ratio is necessary in the larger L\* motor to achieve the same initial depressurization rate as the smaller L\* motor, the final pressures differ in the two cases as do the final portion of the blow-down curves. The larger area ratio is seen to be sufficient to cause the pressure in the larger motor to drop to near ambient, the propellant burning rate dropping to a level consistent with extinguishment. The pressure in the smaller L\* motor levels off at a new steady-state well above ambient with no indication that extinguishment would occur. If the model predicts a response that is truly indicative of the actual response in a motor, as suggested by the comparisons made above, this set of calculations clearly shows the difficulty that might be encountered in correlating data for extinguishment conditions described only in terms of the initial depressurization rate or  $t_k$ . Critical initial rates obtained with end-burning motors which usually have large L\*'s should not be expected to be the same as critical initial rates obtained with motors containing internal burning cylinders, which normally have low L\*'s.

Some data from References 10 and 12 are shown in Figure 11 and tend to confirm the predictions that have been made. That is, the initial depressurization rate required to extinguish a propellant in a given motor may be significantly different from that in a different motor—thus making design on the basis of dP/dt data very difficult.

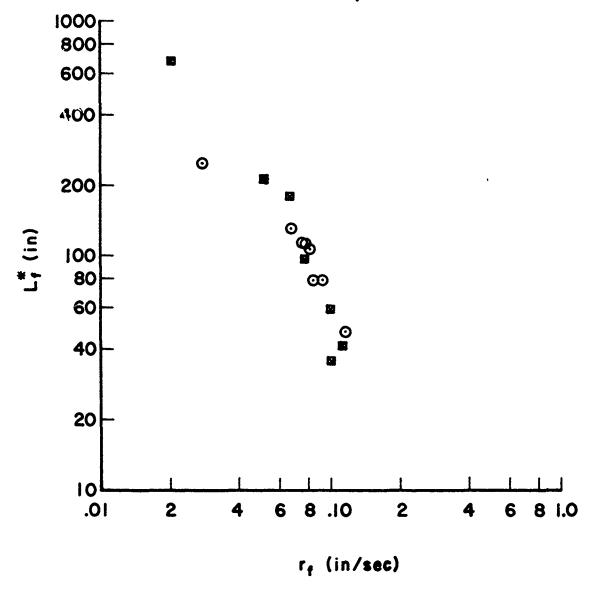


Data taken from References 10 and 12 showing that propellant in different motors requires differenct depressurization rates to be extinguished.

Figure 11

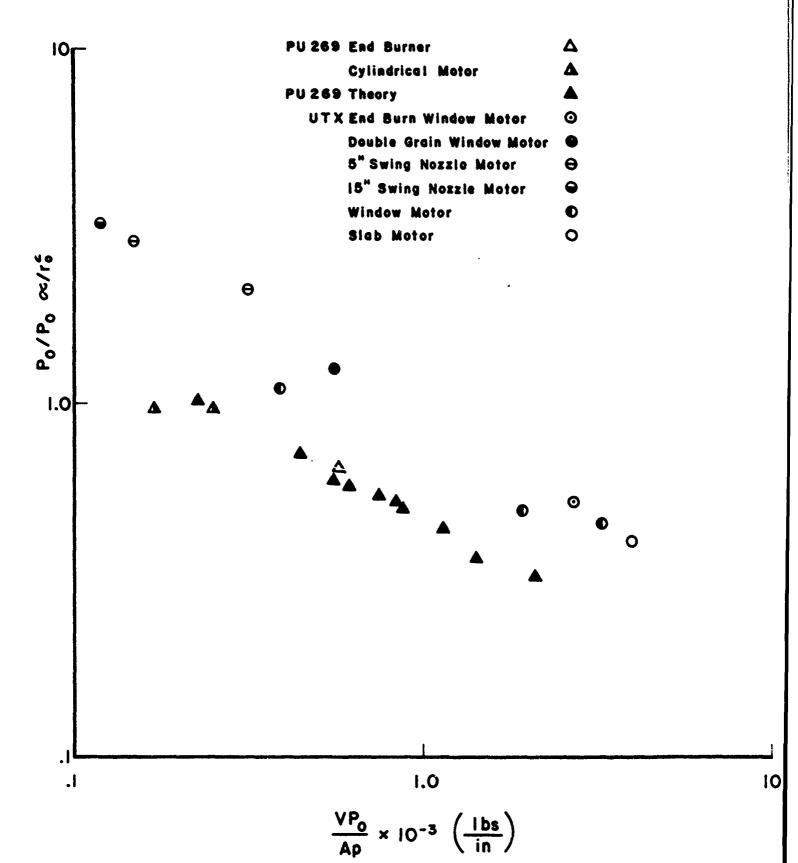
Figure 12 shows that experimental data for the effect of motor size can be correlated and also that the predictions of the improved extinguishment model are in good agreement with the experimental data. However, Figure 12 probably does not represent the best form of correlation that can be made. As is discussed in Reference 16, it appears that a simpler and better correlation relates the final L\* of the motor to the final burning rate. That is, the steady-state burning rate that would result from the increased nozzle area if stable combustion resulted. Figure 13 shows results of the parametric study presented in this type of correlation.





Data taken from Reference (10) and (12) showing a relation between initial pressure (P), depressurization rate (Po), burning rate (), thermal diffusivity (), chamber free volume (v), and exposed propellant surface. (Ap)

Figure 12



Theoretical relationship between the final conditions in a motor that marginally fails to be extinguished, for two types of steady-state burning behavior.

### VI. CONCLUSIONS

- 1. It has been shown that the effect of radiation on the propellant burning rate can be used to evaluate some combustion parameters and the values can then be used to test the consistancy of a combustion model.
- 2. Extinguishment and oscillatory combustion were shown not to be related-at least not in a simple manner.
- An improved extinguishment model has been developed and shown to agree well with experimental data.

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## VIII. SAMPLE COMPUTER PROGRAM

```
MOTOR THRUST TERMINATION
     C
     C
                          HEVISED OCTOSER 1969
            A.I. COATES
1
           COMMON TRRNT(A), U1, J2, J3, NPTS, 1,
                   TO, PA, AH, XKN, ANR, TOPEN, ELSTAR, EPS,
1
1
                   PRAK, RMIN, KNRAR, TERAR, TSRAR, RHOS, GAM, CSTAR,
1
                   FS, EG, CSCG, FEXT, ALPHA,
1
                   CAPGAM, PCRIT, GAMF1, GAMF2, GAMF3, TCHAM, TSOL, HB, DC, TCI,
1
                   Y,P,R,MLPDT,PATE,PRESS,TF,TC,TS,TLAST,DEPTH,AN,XNP,
                   TARLP(A), TABLR(A), RP
2
           COMMON J. TIME (140), PRES (140), TEMP (140), BRATE (144)
 3
            DIMENSION NAME (20)
 4
            REAM (10)0
5
       12
            J≅Ü
            READ (5,13,NAME
Ó
7
       13
           FORMAT (20A4)
8
            WHITE (6, 14) NAME
9
           FORMAT (141,2/44)
       16
10
           N=12
11
            REAM(5,43) TERMY(1), TERMY(2), J1, J2, J3, NETS
12
           FORMAT (2F10.5,412)
13
            TPRMT(3)=TPRMT(1)
14
            TPRNT(5)=TPRNT(1)
15
            TPRVT(4)=2. *TPKNT(2)
            TPRNT(6)=2, *TPHNT(2)
10
            IF(12) 45,45,44
17
18
        44 RFAD(5,48) TARLP
19
            READ(5,40) TARLE
20
        45 READ (5,49) TO, PA, AR, XKN, ANR, TOPEN, ELSTAR, EPS
21
            READ(5,40) REAR, RHIN, XNRAR, TERAR, TSBAR, RHOS, GAM, CSTAR
22
            READ (5,40) FR, EG, CSCG, FEXT, ALPHA
23
       40
            FORMAT (8F10.5)
24
            TSOL = ALPHA/(RHAR+RBAR)
25
            DO 38 [=1,6
26
       30
            TPRMT(I)=TPRNT(I)/TSOL
27
            WPITE (6.42) TO, KRAP, ES, PA, RMIN, EG, AB, XNBAR, CSCG, XKN, TFPAR, FEXT,
       41
27
                          ANR, TSRAR, ALPHA, TOPEN, FHOS, ELSTAR, GAM , EPS, CSTAR
            FOR"AT(1HC, 12Y, 'INPUT DATA'//
28
       42
28
                                 =,F10,3,10x,AHRBAR =,F10,3,10x,6HES
                                                                            = .F12.3/
                     OTHO.XF.S
28
                                                                           =,F10.3/
                                 =,F10,3,10x,6HRHIN =,F18.3,10x,6HEG
                     23X,64PA
38
                                 =,F10.3.10x,6HNBAR =,F10.3.10x,6HCSCG =,F10.5/
                     54X'8474
58
                                 =,F10.3.10x,6HTFPAP=,F10.3,1VX,6HFEXT =,F1V.3/
                     50X, 64K1
28
                     20x, AHANR = =,F10.3, LOX, 6HTSPAR=,F10.3,10x, 6HALPHA=,F10.6/
28
                     20x,64TOPEN=,F10,3,10x,6HRHOS =,F10,3/
85
                     20x,64L5TAR=,F10,3,10x,64GAMMA=,F10.3/
                     20x,6HEPS =,F10,3,10x,6HCSTAR=,F10.3)
28
29
           WRITE (A,80)
           FORMAT (1H3.3Y, TYME!, 4X, PRESSURE!, 3X, DLPDT!, 7X, TRATE!, 5X,
33
       84
           * SRATE 1.5X, TEMPE 1,5X, TEMPC1,5X, TEMPS1,6X, TLAST1,4X, TEMPTH1,
30
10
           +4x, INCZZLE1, 4Y, 'EXPONENT!)
31
            CALL FVFS (N, TPRNT)
32
            IF(J3) 36,36,34
33
       34
            IF(PATE)35,35,36
34
       35
            ANREG. SHANR
35
            N=17
36
            GO TO 44
37
       36
            IF (J1) 60,69,59
38
       50
            WRITE (6,16)NAME
            CALL XYPLOT (J,50,100,3,TIAF,PRES,TEMF,BRATF)
39
```

115, T=10 COATES

FORTRAN DECK MAIN . 1 10/24/05

40 6° G0 Y0 1° 41 RET IPK 42 END

HESSAGES FOR ABOVE COMPILATION.

S VERSION 4 MOD 1

, P

626

```
SUMPOUTINE SETUP (T.Y.SIG.N)
           DIMENSION T(2), Y(20), SIG(20)
           COMMON TRUNT(A). J1. J2. J3. NPTS. I.
3
                   TO, PA, AH, XKN, ANK, TOPEN, ELSTAF, EPS,
5
                   DRAR, RUIN, YHRAR, TERAH, TSRAR, RHOS, GAM, CSTAR,
3
                   FS, EG, CSCG, FFXT, ALPHA,
                   CAPGAM, PCHIT, GAMF1, GAMF2, GAMF3, TCHAM, TSOL, HB, DE, TCI,
3
3
                   Y, P, R, NLPDT, RATE, PRESS, TF, TC, TS, TLAST, DEPTH, AN, XNP,
3
                   TARLP(A), TAHLR(8), PP
           COMMON J, TIME (100), PRES (100), TEMP (100), BRATE (100)
4
                          REFERENCE PRESSURE IS 1000PST
     C
                          DEFERENCE RATE IS PATE AT 1870PSI
     C
                          REFERENCE CONDITIONING TEMP IS 250
     C
                          CALCULATE CONSTANTS
           CAPGAM=GAM+(2./(GAM+1.))++((GAM+1.)/(GAM+1.))
5
           PCRTT=(2./(GAM+1.)) ++(GAM/(GAM-1.))
6
           GAMF1=SORT(2.+GAM/(CAPGAM+(GAY-1.)))
7
8
           GAMF2=2./GAM
           GAMF3=(GAM+1.)/GAM
9
           AA=1.5*(1.0-X43AR)
10
           BR=AA/(1.0-AA)
11
            DD=PHOS+XKN+CSTAR+RPAR/(1000.+32.17)
12
            TCHAM=EI STAR/(CAPGAM+CSTAR+12.+DD)
13
            C1=FG+1000./(2.+1.98)
14
15
            I = 1
16
            M=2
17
            T(1)=2.
                          CALCULATE APPROXIMATE FLAME TEMP
     C
            TO=TO+273.
18
            TFRAD=FFXT+CSCG+TO
19
            TF=TFHAR+CSCG+(TO=298.)+TFRAD
       17
29
            IF(J2) 51,50,52
?1
                          CALCULATE INITIAL PRESSURE, SUMMERFIELD LAW
     C
22
        SE XNP=XNRAR
            RT=(TF/TFPAR)++(1.+XNP)+EXP(+C1+(1./TF+1./TFBAR))
23
            P=(((1.7+RH)+RT+DN-1.)/RH)++1.5
24
            CC=RH+P++C.667
25
            XNP=1.0-E.667+CC/(1.+CC)
26
            RP=P*(1.+R4)/(1.+CC)
27
            R=RT+PP
28
                          ITERATE ON TF
     C
29
        61 TERAS=TERADIA
30
            M=M+1
            IF(4-18) 26,24,27
31
            GO TO 10
32
       26
        27 GC TO 6"
33
                          CALCULATE INITIAL PRESSURE, VIFILE LAW
     C
34
            XNP=XNBAR
       51
            RT=(TF/TFRAR)+*(1.+XNP)*EXP(-C1+(1./TF-1./TFHAR))
35
            P=HT+ND++(1./(!.-XNP))
36
17
            REPERYNP
            G0 TO 61
38
                          CALCULATE INITIAL PRESSURE, P.R TABLE
     C
            P=1202.
        52
39
            R=RDAR/DD
40
            CALL PRATE(P, PP, XYP, TABLP, TABLE, NPTS, 1)
        84
11
            RT=(TF/TFRAR)++(1.+XNP)+EXP(-C1+(1./TF+1./TFBAR))
15
 15
            RP=RT+RP
```

```
215, Taid COATES
                                           FURTHAN DECK SETUP .
                                                                          10/24/65
 44
             IF(ARS(0-RF)-.0005) 35.35.30
 45
         3%
             4××4
 46
             P#1/36. +RP+UD/RRAR
 47
             50 TO 83
 48
         35 Pap/1:04.
  49
             R=R/RHAD
 50
             GO TO 61
      C
                          CALCULATE SOLID TEMPERATURES
 51
          AS TSBAR=TSBAR+275.
 52
             TSETSPAP/(1.-1.98+TSBAR+ALUG(R)/(ES+1000.))
 53
             Y(1)=TS/TO
 54
             T1=1.13 (93+Y(+)-.13393
 55
             Y(2)=2.+Y(1)-T1
 50
             DO 20 1=3.7
 51
        2ª Y([)=>.*Y([-1)-Y([-2)
 58
             Y(8)=(Y(7)+1.)/2.
 59
             Y191=P
 60
             Y(12)=R
 61
             Y(11)=TF/TFBAR
 62
             Y(17)=Y(11)
 63
             TCIETF
 64
             TC=TF
 45
             RETHRN
 66
             END
```

MESSAGES FOR ABOVE COMPILATION.

TÉ

0.26

```
SUBPOUTINE PRATE (P, RP, XNP, TABLE, TABLE, NPTS, 1)
2
           DIMENSION TABLE (8), TABLE (0)
          IF (TABLP(1)-P) 2,4,4
3
 4
           1=1-1
5
           IF (I-1) 3,3,1
           1=1
 6
7
           50 TO 7
          IF /TABLP(1+1)-P) 8,5,5
8
9
          1=1+1
10
           IF (I-NPTS)10,6,6
          I=VPTS-1
11
           G0 T0 7
12
       10
          IF (TABLP(1-1)-P) 7,5,5
13
        7 XMP=ALOG(TABLR(1+1)/TABLR(1))/ALOG(TABLP(1+1)/TABLP(1))
14
15
          RP=TARLO(I)+(P/TAHLP(I))++XNP
16
           RETURN
17
           END
```

) MESSAGES FOR ABOVE COMPILATION.

'EQ

. ...

**#26** 

```
FORTRAN DECK INTERN
                                                                              10/24/~4
            S HADILLIAL DIEED (L'A')ANX ... TENY
 1
            DIMESSION T(2), Y(20), BYOX(2A)
 5
            COMMON TORIT(A), 31, 32, 33, NPTS, 1,
 3
                    TO, PA, AR, XKN, ANR, TOPEN, ELSTAR, EPS,
 5
                    PRAR, PHIM, YNDAP, TERAR, TERAR, RHOS, GAM, CETAR,
                    TS.EG, CSCG, FFXT, ALPHA,
 3
                    CAPGAM, PCHIT, GAMF1, WAMF2, GAMF3, TCHAM, TSOL, HR, DE, TCI,
 3
                    Y,P,R, NLPNT, RATE, PRESS, TF, TC, TS, TLAST, LAPTH, AN, YNP,
 3
                    TARLP(A), TAHLR(B), RP
 4
            COMMON 1, TIME (129), PRES(100), TEMP (120), PRATE(100)
 5
            X=T(1)+TSOL
            P=Y(9)
 7
            R=Y(12)
 d
            RATE=RBAR#Y(10)
 9
            PHESS=1700.4Y(9)
:0
            TF=TFAAR+Y(11)
            TC=TFR49+Y(12)
11
     C
                           CALCULATE NOZZLE AREA
12
            IF (X+TOPFN) 30,30,40
15
       30
            AN=AB/XKN+(1.4+(ANH-1.0)+X/TOPEN)
14
            GP TO 41
15
        4.7
            WENSYXKHARHS
            A = A \times / (PD + AB / XKU)
16
        41
     C
                          CHECK FOR EXTINGUISHMENT
17
            IF (RATE-RMIN) 13,17,20
:8
            RATF=2.
       13
19
            N = 2
22
            CALL PRINT(T, Y, TYDX, N, TPR)
21
            RETURN
22
       24
            CONTINUE
     C
                           CALCULATE SURFACE FLUX
23
            FS==+(Y(1)-1.+CSCS+(TFHAR+T0-298.-TF)/T0)+FFXT
     C
                           CALCULATE SURFACE TEMP CHANGE
24
            T1=V(2)+P.267R6+FS/R
25
            DYDY(1)=56,*R*R*(T1-2.0*Y(1)+Y(2))
     C
                          CALCULATE PATE CHANGE
56
            C?=1300.+FS/(1.98+T0)
            DR=P+C2+DYDX(1)/(Y(1)+Y(1))
27
     C
                          CALCULATE PRESSURE CHANGE
28
            RAC=SORT(TF/TCI)+P+4
       63
29
            PRAT=PA/PRESS
30
            IF(PRAT-PORIT) 55,55,48
            PRATE=PRAT++GAME2-PRAT++GAME3
31
       48
32
            IF (PRATE) 49,49,58
33
       49
            RS=".
34
            G3 TO 51
35
            RS=RNC#FPS#GAMF1#SURT(PRATE)
36
            IF (RS-PNC) 51,51,55
57
       51
            RNERS
            GO TO 79
38
39
       55
            RN=PNC
            DP=TSOL/TCHAM +GAM+TC/TCI+R+(TF/TC+RN/R)
43
       70
     C
                           CALCULATE CHAMBER TEMP CHANGE
41
            TTC=(TSTE/TCHAM)+TC/P+TC/TC(+R+(GAM+TF/TC-1.+(1.-GAM)+RN/P)
42
            IF(.12) 75,76,77
     C
                          CALCULATE RP. XNP SUMMERFIELD LAN
43
       74
            CC=AR+P++C.6A7
```

XNP=1.2-0.667+CC/(1.+CC)

44

5, T=10

COATES

```
45
            kP=P+(1.+RH)/(1.+CC)
46
            GO TO BY
                           CALCULATE RP, XNP
                                                 VIELLE LAW
       75
47
            XYPEXMAR
48
            RP=P++XNP
49
            GC TO 87
                           CALCULATE FP, XNP
                                                 R.P TABLE
53
            P=1700.4P
       77
51
            CALL PRATE(P, RP, XHP, TAHLP, TABLE, NPTS, T)
52
            RP=PP/RDAP
53
            P=P/1889.
54
              GO TO 88
                           CALCULATE FLAME TEMP CHANGE
       87
55
            ETA=1.+YNP+1900.+EG/(3.96+TF)
56
            DTF=TF/FTA+(DR/R-XNP+DP/F)
     C
                           CALCULATE SOLID TEMP CHANGE
57
            \text{NVDY}(2) = 42.*\text{R*R*}(\text{V}(1) = 2.*\text{V}(2) + \text{V}(3)) = 0.4615*(\text{V}(3) = \text{V}(1)) * \text{NR}/\text{V}
58
            DYDY(3)=30.****(Y(2)-2.*Y(3)+Y(4))-0.8442*(Y(4)-Y(2))*DH//
59
            DYDY(4)=20.*R*R*(Y(3)=2.*Y(4)+Y(5))=1.1325*(Y(5)-Y(3))*PR/R
60
            DYDY(5)=12.49+R*(Y(4)=2.4Y(5)+Y(6))=1.3720*(Y(6)-Y(4))+9R/R
61
            DYDY(6)= 6.*R*R*(Y(5)-2.*Y(6)+Y(7))-1.3114*(Y(7)-Y(5))*DR/R
62
            DYDY(7)= 2.*R*R*(Y(6)-2.*Y(7)+Y(8))-1.2619*(Y(8)-Y(6))*PR/x
43
            DYDY(R) = .991 + R + R + (Y(7) - 2.4Y(8) + 1.) - 0.2357 + (1.0 - Y(7)) + DR/R
64
            DYDY(9)=DP
65
            DYDY(18)=DR
66
            DYDY(11)=DTF/TFPAR
67
            DYDY(12)=DTC/TERAR
49
            RETHRA
69
            END
```

FORTHAN DECK 'TIFEO

MESSAGES FOR ABOVE COMPILATION.

17

115.7=12 COATES

10/24/51

```
SHAPO ITTHE PRINT (T.Y. BYDX.N. TPP)
1
            DIMFUSION T(2), Y(23), DYDX(28), TPR(2)
2
            COMMON TPRATICA), J1, J2, J3, HPTS, I,
3
                    TO. PA. AB. XKN. ANH. TOMEN, EL STAF, EPS.
 5
 5
                    PRAW, PMIN, XNHAR, TERAR, TSRAR, FHOS, GAM, CSTAR,
                    FS.EG. OSCG, FEXT, ALPHA.
 3
 3
                    rapgam, porty, game 1, game 2, game 3, toham, tool, hr, DC, tot,
 3
                    Y, P, R, DLPDT, RATE, PRESS, TF, TC, TS, TLAST, DEPTH, AN, XNP,
 3
                    TARLP(A), TABLP(B), HP
 4
            CCMMO: J.TIME(100), PRES(100), TEMP(100), GRATE(100)
 5
            TS=T0+Y/11-273.
            TLAST=TO+Y(A)-275.
 6
 7
            DEPTHEALPHA/RRAP+2.593/R
 8
            DLPDT=DVDY(9)/(P+TSOL)
 9
            SHATE=RPORHAR
           - WHITE (A,15) X.PRESS, DLPDT, RATE, SRATE, TF, TC, TS, TLAST, DEPTH, AM, XMM
10
       14
            FARMAT (F10.5, F10.2, 3F10.4, 2F10.1, 2F10.2, 2F10.5, F10.4)
11
       15
            TSTOP=TPRNT(2)+TSOL
12
13
            IF (X.GF.TSTOP) N=A
14
            J=J+1
            X=(L) AMIT
15
            9=(L)23+9
16
            TFMP(J)=Y(12)
17
            BRATE(J)=R
18
19
            RETHRN
20
            END
```

I MESSAGES FOR ABOVE COMPILATION.

TO VERSION 4 MOP 1

# SRI TEST PU-269 PROPELLANT PA=165 AR=3.4

# INPUT DATA

						مهدمت درد سه ۱۰۰۰. اورو اس
		TO =	25,000-	RBAR *	0,330	, 13 , 13
	Ì	PA =	15,000	RMIN #		1,000
		AR =	8.300	NBAR =		
•		KM =	238,000	TFBAR=		
•••	_	ANR =	3,400	TSBAR=		
	,	TOPFN=	0.001	RHOS #		
		LSTARE	316,000	GAMMA=		
		EPS =	1.000	CSTAR		
				O I AIL	42004000	4.2.
TIME	PPESSURE	DLPDT	RATE	SRATE	TEMPF	TEMPC
Ø,	518.88	0.016			2910.0	
0,00199	403.86	+19E.57	0.2152			2910.0
0,00399	284.59	-160.53			2823.7	2786,1
0.00599	211.61	-136.797		•	2792.1	2637, 2
0,00799	164.05				2763.3	2537.9
0,00999	131.24	-105.100	3 0.1064		2735.0	2474.1
0.01199	107.47	-95,221			2704.7	2434.4
0.01399	89.49	-88.300		0.1055		2409.4
0.01599	75.36	-83.899		0.0954	2671.5	2392.4
0.01799	63.88	-81.772		0.0865		(2377.8)
0,01999	54.26	-81.741		0.0782	2589.9 ·	2361.3
0.02199	46.00	-83.487		0.0704	2538.1	2339.4
0.02399	38.82	-86.321		0.0630	2477.4	2309.6
0.02599	32.57	-89.153		0.0560	2409.6	_2270.8 [
0,02799	27.20	-90.875		0.0495	2339,3	2223.7
0.02999	22.73	-86.587	7 0.0163		2273,3	
0,03199	19.40	-69.930		0.0435	2216.5	2118,2
0.03399	17.28	-45.209		0.0388	2165,7	2072.9
0.03599	16.16	-22.700		0.0356	2114.3	2041.8
0.03799	15.67	-9.825		0.0338	2059.9.	2024.5
0.03999	15.46	-4.672		0.0330		2014.8
0.04199	15.35	-2.700		0.0327	1956,2	2006.8
0.04399	15.28	-1.871	. •	0.0325	1912,9	1997.8
0.04599	15.23	-1.350		0.0324	1875.2	1987.9
0,04799	15.1,9	-1.039		0.0323	1842.2	1977.2.
0.04999	15.17	ů.836	•	0.0323	1813.1	1966.1
0,05199	15.15	-0.560	A	0.0322	1787.0	1954.8
0.05399	15.13			0.0322	1763.7	1943.5
0,05599	15.12	73.591		0.0322		1932.4
0.05799	15,10	-0.426		0.0322	1723.4	_1921.5
0.05999	15.09	ů.336		0.0321	1705.8	1910.8
0.06199	15.09	<b>70.286</b>		0.0321	1689,6	1903.4
0.06399		-0.262		0.0321.	1674,6	1892.2
0.06599	15.08	<b>-0.222</b>		0.0321	1660,7	1882.4
0.06799	15.07	-0.209		0.0321	1647.7	1873.8
Ø. Ø6999	15,07	-0.181	• • • • • • • • • • • • • • • • • • • •	0.0321	1,635,6	1861,5
0.07199	15.06	-0.142		0.0321	1624.3	1852.4
0.07199	15,06	-0.120		0.0321	1613,6	1843.7
	15.05	-0.101		0.0321	1603.5	1835.2
Ø,07599	15.05	-0.084		0.0320	1594,0	1826,9
0,07799	15.05	-0.072		0.0320		1818.9"
0,07999	15.05	-0.048	8 ค.0026	0,0320	1576,4	1811.1
•					• • • •	

ES = 20.000 EG = 20.000 CSCG = 0.750 FEXT = 0. ALPHA= 0.000250

TEMPS 79.95 79.50 0.00257 0.03487 0.4309 568.89 75.66 0.00301 0.11857 0.4457 554.31 70.92 0.00372 0.11857 0.4693 542.34 67.35 0.00445 0.11857 0.4920 531.79 64.46 0.00523 0.11857 0.5337 513.14 59.96 0.00609 0.11857 0.55337 513.14 59.96 0.00609 0.11857 0.55337 513.14 59.96 0.00609 0.11857 0.5529 564.35 564.6 0.00615 0.11857 0.5891 486.39 54.90 0.01318 0.11857 0.6067 476.64 53.41 0.01318 0.11857 0.6067 476.64 53.41 0.01318 0.11857 0.6425 442.89 48.93 0.02492 0.11857 0.6425 442.89 48.93 0.02492 0.11857 0.6614 42.89 48.93 0.02492 0.11857 0.7008 420.05 46.07 0.03961 0.11857 0.7204 44.08 0.06885 0.11857 0.7505 388.75 42.40 0.07892 0.11857 0.7505 388.75 42.40 0.07892 0.11857 0.7618 379.29 41.39 0.09848 0.11857 0.7623 372.07 40.63 0.1261 0.11857 0.7623 372.07 40.63 0.1261 0.11857 0.7623 372.07 40.63 0.113489 0.11857 0.7623 372.07 40.63 0.113489 0.11857 0.7623 372.07 40.63 0.113489 0.11857 0.7623 372.07 40.63 0.113489 0.11857 0.7630 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7636 355.73 38.92 0.17594 0.11857 0.7636 355.73 38.92 0.17594 0.11857 0.7636 355.73 38.92 0.17594 0.11857 0.7637 355.02 38.43 0.19862 0.11857 0.7637 355.02 38.43 0.19862 0.11857 0.7637 355.02 38.43 0.19862 0.11857 0.7637 355.02 38.43 0.19862 0.11857 0.7638 347.09 38.43 0.19862 0.11857 0.7638 347.09 38.43 0.19862 0.11857 0.7638 347.09 38.43 0.19862 0.11857 0.7638 347.09 38.43 0.19862 0.11857 0.7638 347.09 38.43 0.22008 0.11857 0.7638 344.80 37.80 0.23378 0.11857 0.7638 343.74 37.69 0.224705 0.11857 0.7638 342.72 37.59 0.224705 0.11857 0.7638 343.77 37.59 0.224705 0.11857 0.7639						
568.89       75.66       0.00301       0.11857       0.4693         554.31       67.35       0.00445       0.11857       0.4693         531.79       64.46       0.00523       0.11857       0.5337         522.20       62.05       0.00609       0.11857       0.5337         513.14       59.96       0.00705       0.11857       0.5529         50.43       58.12       0.00815       0.11857       0.55891         495.53       56.46       0.00946       0.11857       0.5891         486.39       54.90       0.01518       0.11857       0.6067         476.64       53.41       0.01518       0.11857       0.6244         466.07       51.93       0.01598       0.11857       0.6244         466.07       51.93       0.01598       0.11857       0.6244         442.89       48.93       0.02492       0.11857       0.6809         431.05       47.45       0.03514       0.11857       0.7008         420.05       46.07       0.03501       0.11857       0.7008         421.82       43.88       0.056/2       0.11857       0.7663         384.73       42.40       0.07892 <td< td=""><td>TEMPS</td><td>TLAST</td><td>DEPTH</td><td>NOZZLE</td><td>EXPONENT</td><td></td></td<>	TEMPS	TLAST	DEPTH	NOZZLE	EXPONENT	
554.31       70.92       0.00372       0.11857       0.4693         542.34       67.35       0.00445       0.11857       0.4920         531.79       64.46       0.00523       0.11857       0.5134         522.20       62.05       0.00609       0.11857       0.5529         513.14       59.96       0.00705       0.11857       0.5529         524.35       58.12       0.008315       0.11857       0.5891         495.53       56.46       0.00946       0.11857       0.6067         476.64       53.41       0.01318       0.11857       0.6042         476.64       53.41       0.01318       0.11857       0.6425         454.68       50.44       0.01318       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7008         421.82       43.88       0.056/2       0.11857       0.7496         364.73       43.07       0.06885       0.11857       0.7618         372.07       40.63       0.11712 <t< td=""><td>579,95</td><td>79.50</td><td>•</td><td></td><td></td><td></td></t<>	579,95	79.50	•			
542.34       67.35       0.00445       0.11857       0.4920         531.79       64.46       0.00523       0.11857       0.5134         522.20       62.05       0.00609       0.11857       0.5537         513.14       59.96       0.00705       0.11857       0.5529         524.35       58.12       0.00815       0.11857       0.5891         495.53       56.46       0.00746       0.11857       0.5891         486.39       54.90       0.01318       0.11857       0.6067         476.64       53.41       0.01318       0.11857       0.6425         454.68       50.44       0.01979       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6614         442.80       48.93       0.02492       0.11857       0.6614         442.80       44.89       0.04882       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.77496         374.73       43.07       0.06885       0.11857       0.77496         388.75       42.40       0.07892       0.11857       0.7623         372.07       40.63       0.11712       <	568.89	75.66				
531.79       64.46       0.00523       0.11857       0.5134         522.20       62.05       0.00609       0.11857       0.5337         513.14       59.96       0.00705       0.11857       0.5712         504.35       58.12       0.00815       0.11857       0.5891         495.53       56.46       0.00646       0.11857       0.6067         476.64       53.41       0.01598       0.11857       0.6244         466.37       51.93       0.01598       0.11857       0.6624         446.67       51.93       0.01598       0.11857       0.6642         454.68       50.44       0.01979       0.11857       0.66809         431.05       47.45       0.03961       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7204         410.24       44.08       0.04882       0.11857       0.7565         384.73       43.87       0.06885       0.11857       0.7565         388.75       42.40       0.07892       0.11857       0.7623         383.66       41.85       0.09848       0.11857       0.7623         379.20       41.31       0.12611 <t< td=""><td>554.31</td><td>70.92</td><td></td><td></td><td></td><td></td></t<>	554.31	70.92				
531.79 64.46 0,00523 0,11857 0.5134 522.20 62.05 0,00609 0,11857 0.5337 513.14 59.96 0,00705 0,11857 0.5529 524.35 58.12 0.00815 0,11857 0.5891 486.39 54.90 0.01108 0,11857 0.6067 476.64 53.41 0.01318 0,11857 0.6067 454.68 50.44 0.01979 0,11857 0.6425 454.68 50.44 0.01979 0,11857 0.6614 442.89 48.93 0.02492 0,11857 0.6614 442.89 48.93 0.02492 0,11857 0.66809 431.05 47.45 0.043154 0,11857 0.7008 420.05 46.07 0.03901 0,11857 0.7374 461.82 43.88 0.05672 0,11857 0.7597 388.75 42.40 0.07892 0,11857 0.7595 388.75 42.40 0.07892 0,11857 0.7597 383.66 41.85 0,08881 0,11857 0.7613 379.29 41.39 0.09848 0,11857 0.7626 372.07 40.63 0,11712 0,11857 0.7626 372.07 40.63 0,11712 0,11857 0.7627 372.07 40.63 0,11712 0,11857 0.7629 375.46 40.96 0,10791 0,11857 0.7629 375.46 40.93 0,13489 0,11857 0.7629 366.31 40.03 0,13489 0,11857 0.7629 366.31 40.03 0,13489 0,11857 0.7630 363.82 39.77 0,14346 0,11857 0.7632 361.55 39.53 0,15185 0,11857 0.7634 359.46 39.31 0,16005 0,11857 0.7634 359.46 38.92 0,17594 0,11857 0.7635 359.46 38.75 0,18365 0,11857 0.7637 354.06 38.75 0,18365 0,11857 0.7637 354.06 38.75 0,18365 0,11857 0.7637 349.64 38.29 0.0590 0,11857 0.7637 349.64 38.29 0.0590 0,11857 0.7637 349.64 38.29 0.0590 0,11857 0.7638 347.09 38.43 0,22098 0,11857 0.7638 347.09 37.91 0,22699 0,11857 0.7638 343.74 37.69 0.23378 0,11857 0.7638	542.34	67.35				
513.14         59.96         0,00705         0,11857         0.5529           524.35         58.12         0.00815         0,11857         0.5712           495.53         56.46         0.0046         0,11857         0.6067           476.64         53.41         0.01598         0,11857         0.6067           476.64         53.41         0.01598         0,11857         0.6244           466.07         51.93         0,01598         0,11857         0.6425           454.68         50.44         0,01979         0,11857         0.6425           454.68         50.44         0,01979         0,11857         0.6809           431.05         47.45         0,03961         0,11857         0.6809           431.05         47.45         0,03961         0,11857         0.7204           411.02         44.38         0,04882         0,11857         0.7374           401.82         43.88         0,056/2         0,11857         0.7565           388.75         42.40         0,07892         0,11857         0.7611           379.29         41.39         0,09848         0,11857         0.7628           372.07         40.63         0,11712		64,46				
504.35       58.12       0.00815       0.11857       0.5712         495.53       56.46       0.00946       0.11857       0.5891         486.39       54.90       0.01318       0.11857       0.6067         476.64       53.41       0.01318       0.11857       0.6425         454.68       50.44       0.01979       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6809         431.05       47.45       0.03961       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7374         410.24       4.88       0.04682       0.11857       0.7496         394.73       43.07       0.06885       0.11857       0.7597         383.66       41.85       0.08881       0.11857       0.7618         379.29       41.39       0.09884       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       40.31       0.12611	522.20	62,05	•			
495.53 56.46 0.00946 0.11857 0.5891 486.39 54.90 0.01108 0.11857 0.6067 476.64 53.41 0.01318 0.11857 0.6244 466.07 51.93 0.01598 0.11857 0.6425 454.68 50.44 0.01979 0.11857 0.6614 442.89 48.93 0.02492 0.11857 0.7008 420.05 46.07 0.03961 0.11857 0.7204 410.24 44.88 0.04882 0.11857 0.7374 401.82 43.88 0.056/2 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7597 383.68 41.85 0.08881 0.11857 0.7611 379.29 41.39 0.09848 0.11857 0.7623 372.07 40.63 0.11712 0.11857 0.7623 372.07 40.63 0.11712 0.11857 0.7623 372.07 40.63 0.11712 0.11857 0.7626 369.04 46.31 0.12611 0.11857 0.7626 369.04 46.31 0.12611 0.11857 0.7630 363.82 39.77 0.14346 0.11857 0.7632 361.55 39.53 3.15185 0.11857 0.7633 359.46 39.31 0.16005 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 355.73 38.92 0.17594 0.11857 0.7635 351.02 38.43 0.19862 0.11857 0.7635 351.02 38.43 0.19862 0.11857 0.7637 349.64 38.29 0.0590 0.11857 0.7637 349.64 38.29 0.0990 0.11857 0.7637 349.64 38.29 0.0990 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 345.92 37.91 0.22699 0.11857 0.7638 344.80 37.80 0.22378 0.11857 0.7638 343.74 37.69 0.24047 0.11857 0.7638	513.14	59,96	•			
486.39       54.90       0.01108       0.11857       0.6067         476.64       53.41       0.01318       0.11857       0.6244         466.07       51.93       0.01598       0.11857       0.6425         454.68       50.44       0.01979       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6809         431.05       47.45       0.03154       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7204         410.24       44.38       0.04882       0.11857       0.7374         401.82       43.88       0.058/2       0.11857       0.7565         388.75       42.40       0.07892       0.11857       0.7565         383.68       41.85       0.08881       0.11857       0.7618         379.29       41.39       0.09848       0.11857       0.7623         375.46       40.98       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         363.82       39.77       0.14346       0.11857       0.7633         364.31       40.03       0.13489 <td< td=""><td>564,35</td><td>58,12</td><td></td><td></td><td></td><td></td></td<>	564,35	58,12				
476.64 53.41 0.01318 0.11857 0.6244 466.07 51.93 0.01598 0.11857 0.6425 454.68 50.44 0.01979 0.11857 0.6614 442.89 48.93 0.02492 0.11857 0.6809 431.05 47.45 0.03901 0.11857 0.7008 420.05 46.07 0.03901 0.11857 0.7204 410.24 44.88 0.04882 0.11857 0.7374 401.82 43.88 0.056/2 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7618 379.29 41.39 0.09848 0.11857 0.7618 375.46 40.96 0.10791 0.11857 0.7628 372.07 40.63 0.11712 0.11857 0.7628 366.31 40.03 0.13489 0.11857 0.7630 363.82 39.77 0.14346 0.11857 0.7630 363.82 39.77 0.14346 0.11857 0.7632 361.55 39.53 0.15185 0.11857 0.7633 359.46 39.31 0.16808 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 38.75 0.18365 0.11857 0.7635 359.46 38.75 0.18365 0.11857 0.7635 359.49 38.43 0.19862 0.11857 0.7636 351.02 38.43 0.19862 0.11857 0.7637 349.64 38.29 0.17594 0.11857 0.7637 349.64 38.29 0.17594 0.11857 0.7636 351.02 38.43 0.19862 0.11857 0.7637 349.64 38.29 0.19121 0.11857 0.7637 349.64 38.29 0.19590 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 343.74 37.69 0.23378 0.11857 0.7638 343.74 37.69 0.24047 0.11857 0.7638	495.53	56,46	0,00946			
466.07       51.93       0.01598       0.11857       0.6425         454.68       50.44       0.01979       0.11857       0.6614         442.89       48.93       0.02492       0.11857       0.6809         431.05       47.45       0.03154       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7204         410.24       44.38       0.04882       0.11857       0.7374         401.82       43.88       0.05872       0.11857       0.7565         394.73       43.07       0.06885       0.11857       0.7565         388.75       42.40       0.07892       0.11857       0.7611         379.29       41.39       0.08881       0.11857       0.7618         375.46       40.98       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         363.82       39.77       0.14346       0.11857       0.7630         363.82       39.53       0.1585       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7635         359.46       39.31       0.16005	486.39	54,90	•			
454.68 50.44 0.01979 0.11857 0.6614 442.89 48.93 0.02492 0.11857 0.6809 431.05 47.45 0.03154 0.11857 0.7008 420.05 46.07 0.03961 0.11857 0.7204 410.24 44.88 0.04882 0.11857 0.7374 401.82 43.88 0.058/2 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7565 388.75 42.40 0.07892 0.11857 0.7611 379.29 41.39 0.09848 0.11857 0.7611 379.29 41.39 0.09848 0.11857 0.7623 372.07 40.63 0.11712 0.11857 0.7623 372.07 40.63 0.11712 0.11857 0.7629 369.04 46.31 0.12611 0.11857 0.7629 366.31 40.03 0.13489 0.11857 0.7630 363.82 39.77 0.14346 0.11857 0.7632 361.55 39.53 0.15185 0.11857 0.7633 359.46 39.31 0.16005 0.11857 0.7635 359.46 39.31 0.16005 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 39.31 0.16808 0.11857 0.7635 359.46 38.29 0.17594 0.11857 0.7635 351.02 38.43 0.19862 0.11857 0.7635 351.02 38.43 0.19862 0.11857 0.7637 349.64 38.29 0.19121 0.11857 0.7637 349.64 38.29 0.1950 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 343.74 37.69 0.24047 0.11857 0.7638	476.64	53.41	-			
442.89       48.93       0.02492       0.11857       0.6809         431.05       47.45       0.03154       0.11857       0.7008         420.05       46.07       0.03961       0.11857       0.7204         410.24       44.88       0.04882       0.11857       0.7374         401.82       43.88       0.056/2       0.11857       0.7565         384.73       43.07       0.06885       0.11857       0.7565         388.75       42.40       0.07892       0.11857       0.7597         383.68       41.85       0.08881       0.11857       0.7618         379.29       41.39       0.09848       0.11857       0.7623         375.46       40.96       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7633         369.46       39.31       0.16005       0.11857       0.7635         359.46       39.31       0.16005       0.11857       0.7635         351.02       38.92       0.17594 <td< td=""><td>466.07</td><td>51.93</td><td>•</td><td></td><td></td><td></td></td<>	466.07	51.93	•			
431.05	454.68	50.44				
420.05       46.07       0.03961       0.11857       0.7204         410.24       44.38       0.04882       0.11857       0.7374         401.82       43.88       0.058/2       0.11857       0.7496         364.73       43.07       0.06885       0.11857       0.7565         388.75       42.40       0.07892       0.11857       0.7597         383.68       41.85       0.08881       0.11857       0.7611         379.29       41.39       0.09848       0.11857       0.7623         375.46       40.96       0.10791       0.11857       0.7626         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16005       0.11857       0.7635         354.06       38.75       0.1857       0.7635       0.7635         354.06       38.75       0.1857       0.	442.89	48.93				
410.24	431.05	47,45	•			
410.24		46.07	•	-		
394.73		44.88	0.04882	0,11857		
388.75       42.40       0.07892       0.11857       0.7597         383.68       41.85       0.08881       0.11857       0.7611         379.29       41.39       0.09848       0.11857       0.7623         375.46       40.96       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7638         347.09       38.03       0.22008	461.82	43,88	0,058/2	•		
383.68       41.85       0.08881       0.11857       0.7611         379.29       41.39       0.09848       0.11857       0.7623         375.46       40.96       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22008	394.73	43.07	0.06885			
383.68       41.85       0.08881       0.11857       0.7611         379.29       41.39       0.09848       0.11857       0.7618         375.46       40.98       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.19590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22008 <td< td=""><td>388.75</td><td>42.40</td><td></td><td></td><td></td><td></td></td<>	388.75	42.40				
375.46       40.98       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7630         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378		41.85	0,08881			
375.46       40.98       0.10791       0.11857       0.7623         372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7639         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047	379.29	41.39	0,09848			
372.07       40.63       0.11712       0.11857       0.7626         369.04       46.31       0.12611       0.11857       0.7629         366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.19121       0.11857       0.7637         349.64       38.29       0.25378       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         347.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047 <td< td=""><td>375.46</td><td>40.98</td><td>0,10791</td><td></td><td></td><td></td></td<>	375.46	40.98	0,10791			
366.31       40.03       0.13489       0.11857       0.7630         363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.19590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047       0.11857       0.7638		40,63	0,11712	•		
363.82       39.77       0.14346       0.11857       0.7632         361.55       39.53       0.15185       0.11857       0.7634         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.19862       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047       0.11857       0.7638	369.04	46.31	0,12611			
361.55       39.53       0.15185       0.11857       0.7633         359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22008       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047       0.11857       0.7638	366.31	40.03		_		
359.46       39.31       0.16005       0.11857       0.7634         357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047       0.11857       0.7638	363.82	39.77				
357.53       39.11       0.16808       0.11857       0.7635         355.73       38.92       0.17594       0.11857       0.7635         354.06       38.75       0.18365       0.11857       0.7636         352.49       38.59       0.19121       0.11857       0.7636         351.02       38.43       0.19862       0.11857       0.7637         349.64       38.29       0.0590       0.11857       0.7637         348.33       38.16       0.21305       0.11857       0.7638         347.09       38.03       0.22098       0.11857       0.7638         345.92       37.91       0.22699       0.11857       0.7638         344.80       37.80       0.23378       0.11857       0.7638         343.74       37.69       0.24047       0.11857       0.7638		39.53		•		
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351.02 38.43 0.19862 0.11857 0.7637 349.64 38.29 0.0590 0.11857 0.7637 348.33 38.16 0.21305 0.11857 0.7638 347.09 38.03 0.22008 0.11857 0.7638 345.92 37.91 0.22699 0.11857 0.7638 344.80 37.80 0.23378 0.11857 0.7638 343.74 37.69 0.24047 0.11857 0.7638	354.06	38.75				
349.64     38.29     0 ^0590     0.11857     0.7637       348.33     38,16     0.21305     0.11857     0.7638       347.09     38.03     0.22098     0.11857     0.7638       345.92     37.91     0.22699     0.11857     0.7638       344.80     37.80     0.23378     0.11857     0.7638       343.74     37.69     0.24047     0.11857     0.7638	352.49	38.59		-		
348.33     38.16     0.21305     0.11857     0.7638       347.09     38.03     0.22098     0.11857     0.7638       345.92     37.91     0.22699     0.11857     0.7638       344.80     37.80     0.23378     0.11857     0.7638       343.74     37.69     0.24047     0.11857     0.7638	351.02	38,43				
347.09     38.03     0.22098     0.11857     0.7638       345.92     37.91     0.22699     0.11857     0.7638       344.80     37.80     0.23378     0.11857     0.7638       343.74     37.69     0.24047     0.11857     0.7638	349.64	ĭ8.29				
347.09     38.03     0.22098     0.11857     0.7638       345.92     37.91     0.22699     0.11857     0.7638       344.80     37.80     0.23378     0.11857     0.7638       343.74     37.69     0.24047     0.11857     0.7638		38,16				
345.92     37.91     0.22699     0.11857     0.7638       344.80     37.80     0.23378     0.11857     0.7638       343.74     37.69     0.24047     0.11857     0.7638		38.03		•		
344.80 37.80 0.23378 0.11857 0.7638 343.74 37.69 0.24047 0.11857 0.7638		37,91				
0.1053	344.80					
342.72 37.59 0.24705 9.11857 0.7639	343.74	37.69	•			
	342.72	37.59	0.24705	9,11857	0.7639	-

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### 1X. PRESENTATIONS AND PUBLICATIONS

"Propellant Extinction," Presented at 3rd AFOSR combined Contractor's Meeting, Cocoa Beach, Florida, June 1967.

"Depressurization Induced Extinction of Burning Solid Propellant," by Horton, et.al., AIAA J. 2, 1968.

"Design Considerations for Combustion Stability," presented at ICRPG/AIAA 3rd Solid Propulsion Conference, Atlantic City, New Jersey, June, 1968.

"Design Considerations for Combustion Stability," by R. L. Coates and M. D. Horton, Journal of Spacecraft and Rockets, 6, 1969.

"Extinction of Burning Solid Propellants," Presented at 5th AFOSR Combined Contractor's Meeting, Denver, Colorado, June 1969.

"The Effect of Radiant Energy on the Burning Rate of a Composite Solid Propellant," by M. D. Horton and L. B. Youngberg, submitted to AIAA Journal.

"Prediction of Conditions Leading to Extinguishment," Presented at 6th ICRPG Solid Propellant Combustion Conference, Pasadena, California, October 1969.

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13. ABSTRACT					
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This report presents a transient combustion quenching of burning solid propellants. The	n model and he model com				
quenching of burning solid propellants. The combustion model of Dennison and Baum with					
state burning rate relationship. Comparison					
model correctly describes the quenching pro					
effects that were previously unexplained.	/	mha!	<del></del>		
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Security Classification LINK C LINK B LINK A KEY WORDS HOLE ROLE Extinction Termination Transient solid propellant combustion Quenching

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